

In the Claims

WHAT IS CLAIMED IS:

1. (Currently Amended) A method for removing organic sulfur compounds from a vent gas stream wherein said vent gas stream comprises air, said method comprising the following steps:

contacting the vent gas stream with liquid hydrocarbon stream; and

absorbing a portion of the organic sulfur compounds from the vent gas stream into the liquid hydrocarbon stream to form an exiting vent gas stream.
2. (Original) The method as described in claim 1, wherein the liquid hydrocarbon stream comprises one or more liquid hydrocarbons.
3. (Original) The method as described in claim 2, wherein the hydrocarbon stream comprises two or more liquid hydrocarbons.
4. (Original) The method as described in claim 1, wherein at least one of the liquid hydrocarbons having a boiling point of between about 180°F and about 430°F.
5. (Currently Amended) The method as described in claim 4, wherein the at least one of the liquid hydrocarbons comprises a compound selected from the group consisting of benzene, xylenes, toluene, hexane, heptane, octane, nonane, or and mixtures thereof.
6. (Currently Amended) The method as described in claim 4, wherein ~~the said~~ at least one of the liquid hydrocarbons comprises a hydrogenated naphtha.

7. (Original) The method as described in claim 1, wherein the sulfur concentration of the exiting vent gas stream is less than one percent of the sulfur concentration of the vent gas stream.

8. (Original) The method as described in claim 7, wherein the sulfur concentration is less than 0.5% of the sulfur concentration of the vent gas stream.

9. (Currently Amended) The method of claim 1 further comprising
after step (b):
hydrotreating the hydrocarbon stream.

10. (Currently Amended) The method of claim 1 further comprising
after step (b):
routing the exiting vent gas stream to an incinerator or a heater.

11. (Original) The method of claim 1, wherein the organic sulfur compound removed is a sulfide.

12. (Original) The method of claim 11, wherein the organic sulfur compound removed is a disulfide oil.

13. (Original) A method for removing organic sulfur compounds from a vent gas stream having organic sulfur compounds, the vent gas stream further having an initial organic sulfur compound concentration, comprising the following steps:

(a) providing a scrubber, the scrubber having a shell, the shell having an interior cavity, a diameter, a vent gas entry port, a vent gas exit port, and a hydrocarbon entry port;

(b) introducing a hydrocarbon stream into a scrubber through the hydrocarbon entry port;

- (c) introducing the vent gas stream into the scrubber through the vent gas entry port;
- (d) absorbing a portion of the organic sulfur compounds from the vent gas stream into the hydrocarbon stream to form an exiting vent gas stream; and
- (e) removing the exiting vent gas stream from the scrubber through the vent gas exit port.

14. (Original) The method of claim 13, wherein the scrubber further comprises gas/liquid contact material, the gas/liquid contact material within the interior cavity of the scrubber.

15. (Currently Amended) The method of claim 14, wherein the gas/liquid contact material comprises a material selected from the group consisting of packing, trays, ~~or~~ and fiber film contactor.

16. (Currently Amended) The method of claim 15, wherein the gas/liquid contact material comprises a material selected from the group consisting of structured packing ~~or~~ and ring-shaped packing.

17. (Currently Amended) The method of claim 16, wherein the gas/liquid contact material comprises a material selected from the group consisting of either raschig rings ~~or~~ and nutter rings, the ~~raschig rings or nutter~~said rings having a diameter.

18. (Currently Amended) The method of claim 17, wherein the ~~raschig rings or nutter~~said rings are comprised of a material selected from the group consisting of carbon steel, stainless steel, carbon, ~~or~~ and ceramic.

19. (Currently Amended) The method of claim 17, wherein ~~the raschig rings or nutters~~said rings have a nominal diameter of between ½" and 2".

20. (Original) The method of claim 14, wherein the scrubber further comprises a packing support, the packing support located within the interior cavity of the shell and able to support the gas/liquid contact material.

21. (Original) The method of claim 13, wherein the diameter of the shell is between about 6" and 24".

22. (Currently Amended) The method of claim 13, wherein the shell comprises a material selected from the group consisting of carbon steel, stainless steel, and Ceramic, RO-AN Inconel alloy.

23. (Original) The method of claim 13, wherein the scrubber further comprises a liquid distributor, the liquid distributor located within the interior cavity of the shell and in the same plane as the diameter of the shell, the liquid distributor further being within functional proximity of the hydrocarbon entry port.

24. (Original) The method of claim 13, wherein the vent gas entry port of the scrubber is mounted on a disulfide separator.

25. (Currently Amended) A method for removing disulfide oils from a vent gas stream having disulfide oils, comprising the following steps:

(a) providing a scrubber, the scrubber having a shell, the shell having an interior cavity, a diameter, a vent gas entry port, a vent gas exit port, a hydrocarbon entry port, and gas/liquid contact material, the gas/liquid contact material located within the interior cavity of the scrubber;

(b) introducing a hydrocarbon stream into the scrubber through the hydrocarbon entry port, the hydrocarbon stream comprising ~~a~~at least one hydrocarbon, the at least one hydrocarbon having a boiling point of between about 180°F and about 430°F;

(c) introducing the vent gas stream into the scrubber through the vent gas entry port;

(d) absorbing a portion of the disulfide oils from the vent gas stream into the hydrocarbon stream to form an exiting vent gas stream; and

(e) removing the exiting vent gas stream from the scrubber through the vent gas exit port.